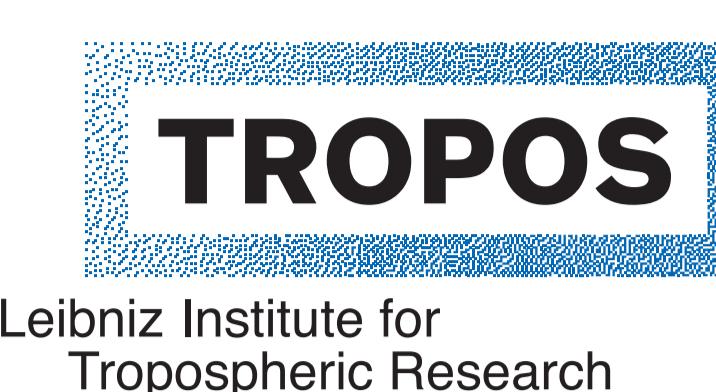


# $\text{H}_2\text{SO}_4$ formation from the gas-phase reaction of stabilized Criegee Intermediates with $\text{SO}_2$ : Influence of water vapour content and temperature

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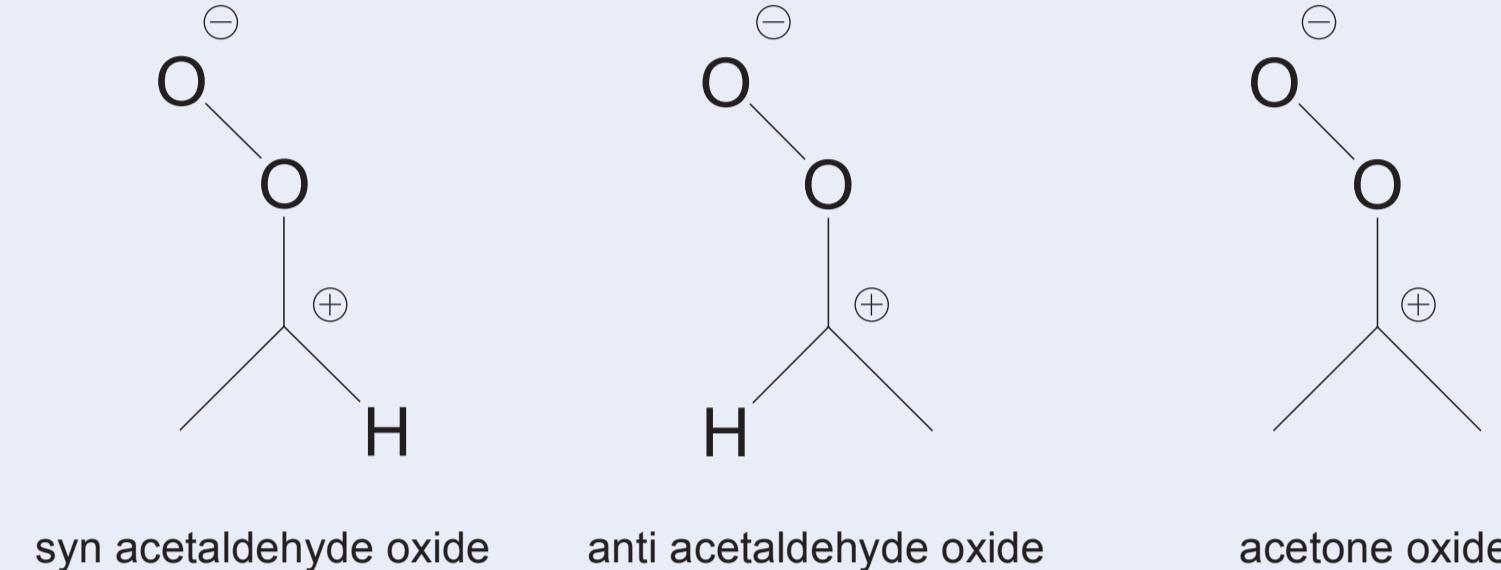
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## Motivation

Very recently, it was discovered that the reaction of sCl with  $\text{SO}_2$  is surprisingly fast and contributes significantly to atmospheric  $\text{H}_2\text{SO}_4$  formation beside the well-known process via  $\text{OH} + \text{SO}_2$  (Welz et al., 2012; Mauldin et al., 2012). Modelling results, however, call a substantial  $\text{H}_2\text{SO}_4$  formation from sCl into question and point to the predominate fate of sCl in the reaction with  $\text{H}_2\text{O}$  vapour (Sarwar et al., 2013). For a reliable assessment of these processes the reactivity of a series of important sCl toward atmospherically relevant trace gases has to know. But, up to now the knowledge is very sparse regarding the needed rate coefficients. Rate coefficients for the reaction of sCl with  $\text{H}_2\text{O}$  vapour,  $\text{SO}_2$  or other trace gases are available for the simplest sCl, formaldehyde oxide ( $\text{CH}_2\text{OO}$ ), and in only few cases for acetaldehyde oxide ( $\text{CH}_3\text{CHO}$ ) (Calvert et al., 1978; Welz et al., 2012; Taatjes et al., 2013). Indirect approaches based on end-product analysis or sCl titration were mostly used due to experimental difficulties of direct sCl probing (Calvert et al., 2000; Fenske et al., 2000; Berndt et al., 2012). Up to now, only a low-pressure experiment at 4 torr allows the direct monitoring of Criegee Intermediates (Welz et al., 2012; Taatjes et al., 2013). It is to be noted that there exist large discrepancies in the absolute values of the sCl rate coefficients, also for the important reactions with  $\text{H}_2\text{O}$  vapour and  $\text{SO}_2$ . Subject of this work are investigations on  $\text{H}_2\text{SO}_4$  formation from the reaction of acetaldehyde oxide (syn- and anti-conformer,  $\text{CH}_3\text{CHO}$ ) and acetone oxide ( $(\text{CH}_3)_2\text{COO}$ ) with  $\text{SO}_2$  for atmospheric conditions in a relatively wide range of the water vapour content in the temperature range 278 - 343 K. Criegee Intermediates are formed via gas-phase ozonolysis of trans-2-butene and 2,3-dimethyl-2-butene (TME).



## Experiment

Institute for Tropospheric Research -

Laminar Flow Tube, TROPOS-LFT:

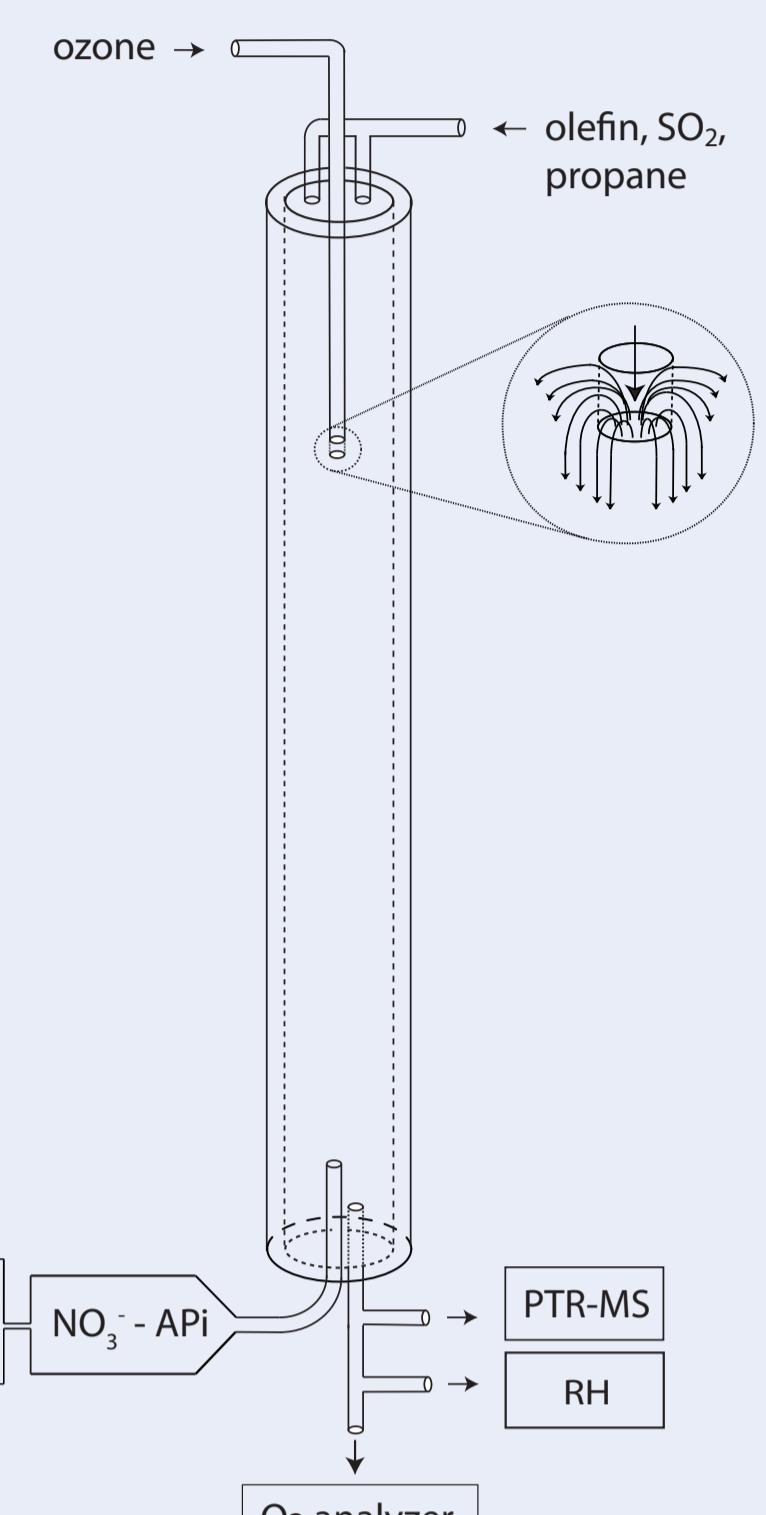
- length: 505 cm, 8 cm i.d.
- carrier gas: purified air (99.999999 vol%)
- atmospheric pressure
- temperature: 278 - 343 K
- flow: 30 l min<sup>-1</sup> (STP), residence time: 39.5 sec.
- $\text{H}_2\text{O}$  vapour: 0.047 - 1.17 vol%

- reactant concentrations:

- [trans-2-butene] =  $4.0 \cdot 10^{10}$  cm<sup>-3</sup>
- [2,3-dimethyl-2-butene] =  $1.0 \cdot 10^{10}$  cm<sup>-3</sup>
- [ $\text{O}_3$ ] =  $(2.0 - 2.2) \cdot 10^{11}$  cm<sup>-3</sup>
- [ $\text{SO}_2$ ] =  $(2.9 - 3300) \cdot 10^{11}$  cm<sup>-3</sup>
- [ $\text{C}_3\text{H}_8$ ] =  $(4.1 - 16.4) \cdot 10^{15}$  cm<sup>-3</sup> (OH scavenger)
- olefin conversion: < 2%

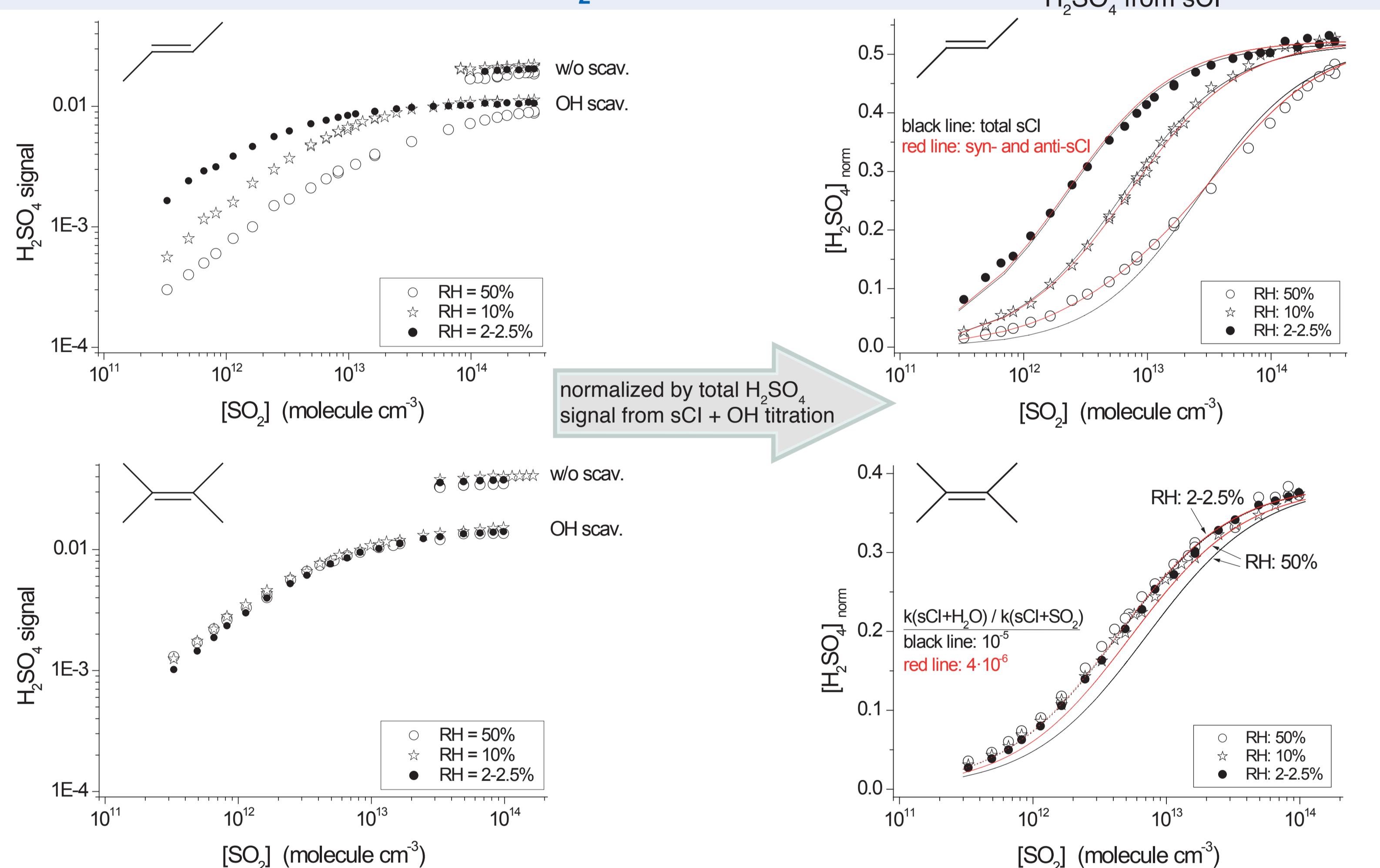
$\text{H}_2\text{SO}_4$  detection:  $\text{NO}_3^-$ -CI-API-TOF

- $\text{H}_2\text{SO}_4$  signal:  $S = \frac{[\text{HSO}_4^-] + ([\text{HNO}_3](\text{HSO}_4^-))}{([\text{NO}_3^-] + ([\text{HNO}_3](\text{NO}_3^-)) + ([\text{HNO}_3^2](\text{NO}_3^-))}$
- calibration factor:  $(1.85 \pm 0.83) \cdot 10^9$  cm<sup>-3</sup>
- detection limit:  $4 \cdot 10^4$  cm<sup>-3</sup> (5 min. integration)



## Results and Discussion

### Experiments at 293 K, variable $\text{H}_2\text{O}$ vapour content



Mechanism (simplified):

- $\text{O}_3 + \text{olefin} \rightarrow y_1\text{OH}(\text{prompt}) + y_2\text{sCl} + \text{others}$  (1)
- $\text{sCl} + \text{H}_2\text{O} \rightarrow \text{products}; k(\text{sCl} + \text{H}_2\text{O})$  (2)
- $\text{sCl} + \text{SO}_2 \rightarrow \dots \rightarrow \text{H}_2\text{SO}_4; k(\text{sCl} + \text{SO}_2)$  (3)
- $\text{sCl} \rightarrow \text{OH} + \text{others}; k(\text{dec.})$  (4)

$$y_2: 0.49 \pm 0.22 \text{ (trans-2-butene)} \text{ and } 0.45 \pm 0.20 \text{ (TME)}$$

$$y_1 + y_2: 0.92 \pm 0.42 \text{ (trans-2-butene)} \text{ and } 1.20 \pm 0.54 \text{ (TME)}$$

$$[\text{H}_2\text{SO}_4]_{\text{norm}} = 1 / (1 + k(\text{dec.}) / (k(\text{sCl} + \text{SO}_2)[\text{SO}_2]) + k(\text{sCl} + \text{H}_2\text{O})[\text{H}_2\text{O}] / (k(\text{sCl} + \text{SO}_2)[\text{SO}_2])) \cdot f \quad (\text{Eq. I})$$

Acetaldehyde oxide (trans-2-butene ozonolysis):

one component (sCl) model (black line):

$$k(\text{dec.}) / k(\text{sCl} + \text{SO}_2) = (1.2 \pm 0.1) \cdot 10^{12} \text{ molecule cm}^{-3}$$

$$k(\text{sCl} + \text{H}_2\text{O}) / k(\text{sCl} + \text{SO}_2) = (8.8 \pm 0.4) \cdot 10^{-5} \Rightarrow 6.1 \cdot 10^{-5} \text{ from literature: Calvert et al., 1978.}$$

two component (syn- and anti-sCl) model (red line):

$$\text{anti: } k(\text{dec.}) / k(\text{sCl} + \text{SO}_2) = (2.7 \pm 1.7) \cdot 10^{11} \text{ molecule cm}^{-3}$$

$$\text{anti: } k(\text{sCl} + \text{H}_2\text{O}) / k(\text{sCl} + \text{SO}_2) = (1.4 \pm 0.1) \cdot 10^{-4}$$

$$\text{syn: } k(\text{dec.}) / k(\text{sCl} + \text{SO}_2) = (3.3 \pm 0.5) \cdot 10^{12} \text{ molecule cm}^{-3}$$

⇒ reaction with  $\text{H}_2\text{O}$  vapour neglected

⇒ Analysis points to a preferred formation of the anti-conformer !

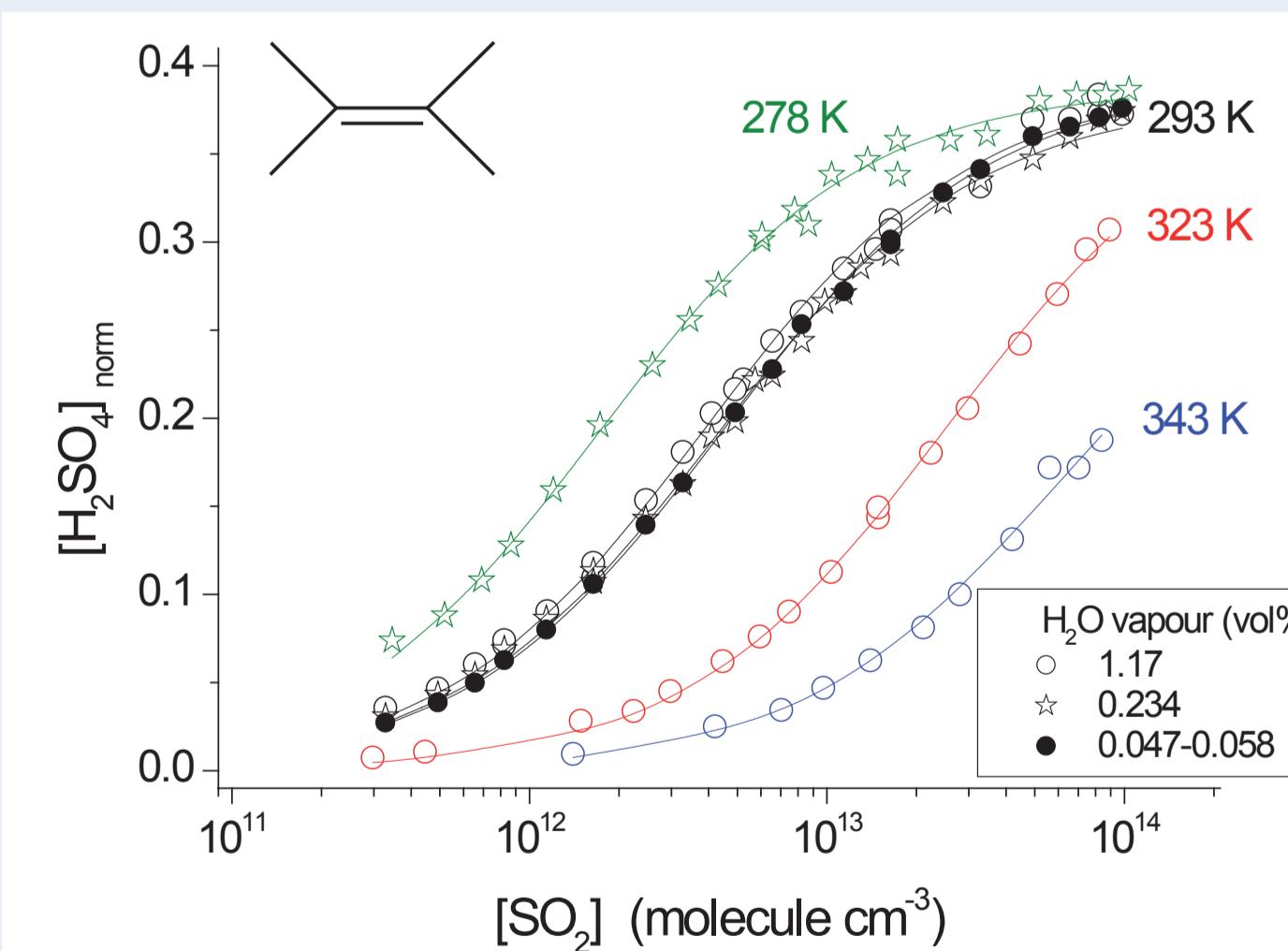
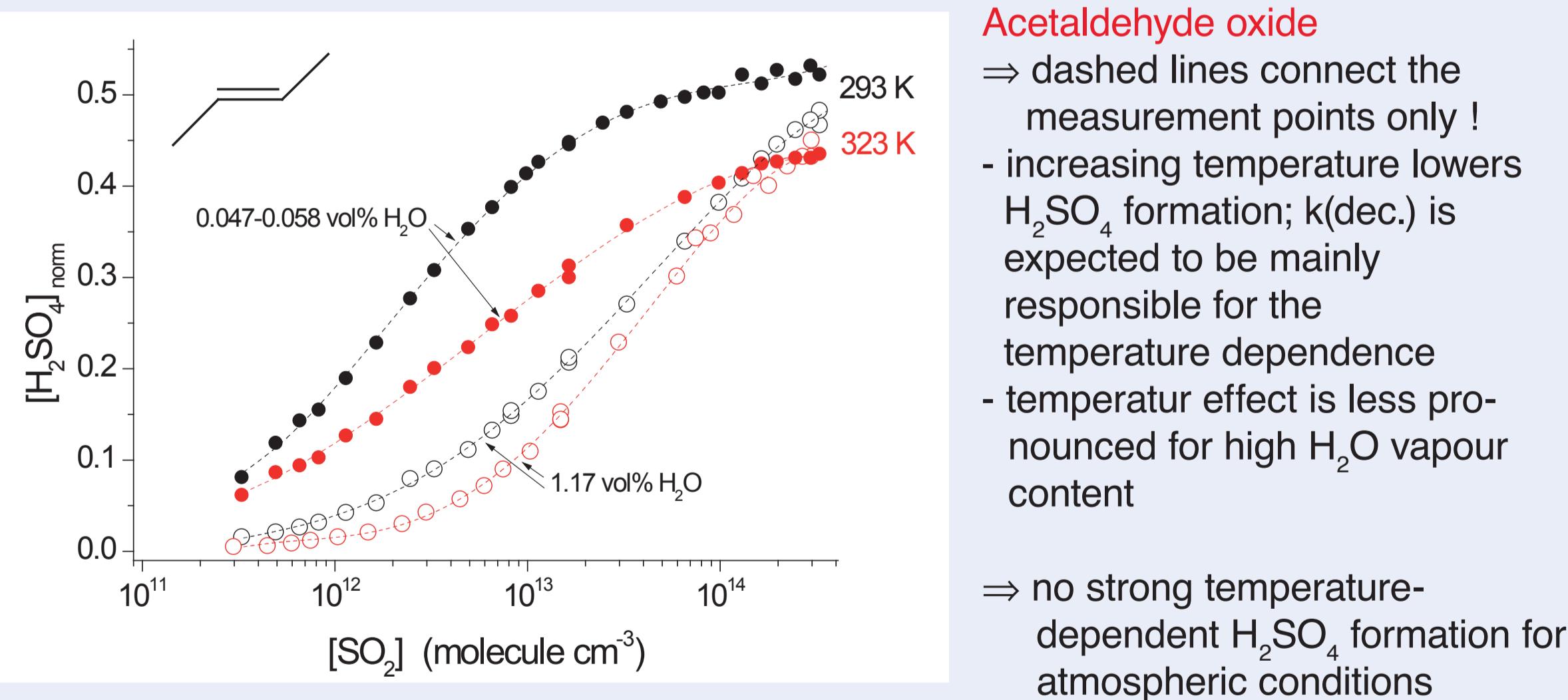
Acetone oxide (TME ozonolysis):

$$k(\text{dec.}) / k(\text{sCl} + \text{SO}_2) = (4.2 \pm 0.3) \cdot 10^{12} \text{ molecule cm}^{-3}$$

$$k(\text{sCl} + \text{H}_2\text{O}) / k(\text{sCl} + \text{SO}_2) < 4 \cdot 10^{-6} \Rightarrow \text{only upper limit estimation possible}$$

⇒ Reaction of sCl with  $\text{H}_2\text{O}$  vapour is strongly dependent on the sCl structure !

### Experiments in the temperature range 278 - 343 K



Acetaldehyde oxide

⇒ full lines show modelling results according to Eq. I (w/o  $\text{H}_2\text{O}$  reaction)

- competition between the reaction of sCl with  $\text{SO}_2$  vs. decomposition describes very well the measurements independent of  $\text{H}_2\text{O}$  vapour

-  $k(\text{dec.}) / k(\text{sCl} + \text{SO}_2)$ :

$$278 \text{ K: } (1.8 \pm 0.5) \cdot 10^{12} \text{ molecule cm}^{-3}$$

$$293 \text{ K: } (4.2 \pm 0.3) \cdot 10^{12} \text{ molecule cm}^{-3}$$

$$323 \text{ K: } (2.5 \pm 0.9) \cdot 10^{13} \text{ molecule cm}^{-3}$$

$$343 \text{ K: } (6.0 \pm 0.8) \cdot 10^{13} \text{ molecule cm}^{-3}$$

- Arrhenius parameter  $\ln(k(\text{dec.}) / k(\text{sCl} + \text{SO}_2))$  vs.  $1/T$

$$E_{a,4} - E_{a,3} = 44.0 \pm 1.2 \text{ kJ mol}^{-1}$$

$$\ln(A_4/A_3) = 47.5 \pm 0.5$$

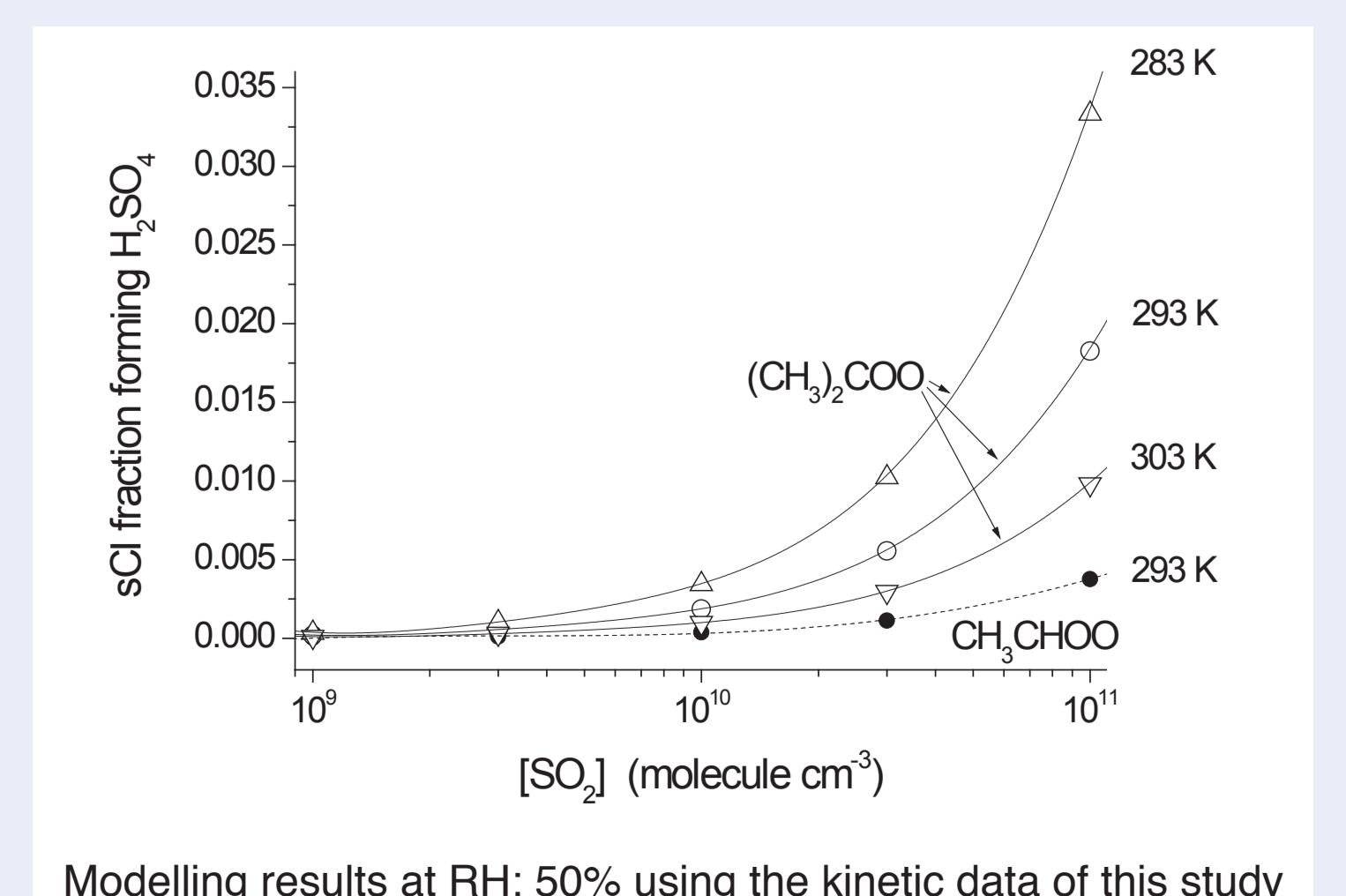
⇒ strong temperature-dependent  $\text{H}_2\text{SO}_4$  formation for atmospheric conditions

## References

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## Summary

- ⇒ acetaldehyde oxide and acetone oxide show different reactivity toward  $\text{H}_2\text{O}$  vapour
- ⇒ atmospheric fate of acetaldehyde oxide is governed by the reaction with  $\text{H}_2\text{O}$  vapour, for acetone oxide thermal decomposition is most important
- ⇒ increasing temperature results in a decrease of  $\text{H}_2\text{SO}_4$  formation (T-dependence of  $k(\text{dec.})$ ), for acetaldehyde oxide only small effects due to the dominate reaction with  $\text{H}_2\text{O}$  vapour for acetone oxide a decrease of  $k(\text{dec.}) / k(\text{sCl} + \text{SO}_2)$  by a factor of 34 increasing the temperature from 278 to 343 K
- ⇒ sCl reactivity and atmospheric fate is sCl-structure dependent



Modelling results at RH: 50% using the kinetic data of this study